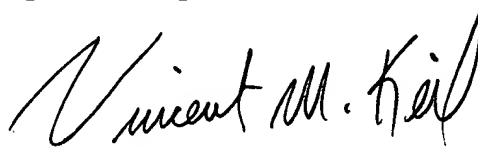


REMARKS

The above amendments have been made to remove multiple claim dependencies and for greater consistency. Upon entry of this amendment, claims 1-29 will be pending in the application.

* Attached hereto is a marked-up version of the changes made to the claims by this amendment. The attached pages are captioned "Version With Markings to Show Changes Made."

Respectfully submitted,



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*Attachment

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VERSION WITH MARKINGS TO SHOW CHANGES MADE

IN THE CLAIMS:

Claims 5-29 have been amended as follows:

5 (amended). A process according to [any one of claims 2 to 4, in which] claim 2, wherein the dehydrogenation catalyst is a copper containing catalyst which comprises, before reduction, copper oxide on alumina.

6 (amended). A process according to [any one of claims 2 to 5, in which] claim 2, wherein the rate of supply of the C₂ feedstock to the dehydrogenation zone corresponds to an ethanol liquid hourly space velocity (LHSV) of from about 0.5 hr⁻¹ to about 1.0 hr⁻¹.

7 (amended). A process according to [any one of claims 1 to 6 in which] claim 1, wherein the selective hydrogenation conditions of step (c) include use of a reaction product mixture:hydrogen molar ratio of from about 1000:1 to about 1:1, a combined partial pressure of the liquefiable products of the intermediate reaction product mixture and hydrogen of from about 5 bar (5 x 10⁵ Pa) to about 80 bar (8 x 10⁶ Pa), and a temperature in the range of from about 20°C to about 160°C.

8 (amended). A process according to claim [78, in which] 1, wherein the combined partial pressure of the liquefiable products

9 (amended). A process according to [any one of claims 1 to 8,
in which] claim 1, wherein the selective hydrogenation catalyst
comprises a metal selected from nickel, palladium, platinum,
ruthenium, rhodium and rhenium.

11 (amended). A process according to [any one of claims 1 to 10,
in which] **claim 1, wherein** the rate of supply of liquefiable
liquid products of the intermediate reaction product mixture to
the selective hydrogenation zone corresponds to a liquid hourly
space velocity (LHSV) of from about 0.5 hr⁻¹ to about 2.0 hr⁻¹.

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and water, supplying material of the first distillate to a second distillation zone maintained under distillation conditions effective for distillation therefrom of a second distillate comprising ethanol, water, and ethyl acetate and so as to yield a substantially pure ethyl acetate bottom product, and recovering a substantially pure ethyl acetate bottom product from the second distillation zone.

13 (amended). A process according to claim 12, [in which] wherein the first distillation zone is operated at a pressure of less than about 4 bar (4×10^5 Pa).

14 (amended). A process according to claim 12 [or claim 13, in which] , wherein the first distillation zone is operated at a pressure of from about 1 bar (10^5 Pa) to about 2 bar (2×10^5 Pa).

15 (amended). A process according to [any one of claims 12 to 14, in which] claim 12, wherein the second distillation zone is operated at a pressure of from about 4 bar (4×10^5 Pa) to about 25 bar (2.5×10^6 Pa).

16 (amended). A process according to [any one of claims 12 to 15, in which] claim 12, wherein the second distillation zone is operated at a pressure of from about 9 bar (9×10^5 Pa) to about 15 bar (1.5×10^6 Pa).

17 (amended). A process according to [any one of claims 12 to 16, in which] claim 12, wherein the first distillate contains less than about 10 mol % water.

18 (amended). A process according to [any one of claims 12 to 17, in which] claim 12, wherein an ethanol rich stream containing substantially all of the water in the selectively hydrogenated reaction product mixture is recovered from the bottom of the first distillation zone, while an overhead stream that contains "light" components present in the selectively hydrogenated reaction product mixture is recovered from the first distillation zone, and in which the first distillate comprises a liquid draw stream which is recovered from an upper region of the first distillation zone and which comprises ethyl acetate, ethanol, water and minor amounts of other components.

19 (amended). A process according to claim 18, [in which] wherein the liquid draw stream contains from about 40 mol % to about 55 mol % ethyl acetate, from about 1 mol % to about 6 mol % water, not more than about 1 mol % other components, and the balance ethanol.

20 (amended). A process according to claim 19, [in which] wherein the liquid draw stream contains about 45 mol % ethyl acetate, about 50 mol % ethanol, about 4 mol % water and about 1 mol % other components.

21 (amended). A process according to [any one of claims 18 to 20, in which] claim 18, wherein the liquid draw stream is passed to the second distillation zone which is operated at a pressure of from about 4 bar (4×10^5 bar) absolute to about 25 bar (2.5×10^6 Pa) absolute.

22 (amended). A process according to claim 21, [in which] wherein the bottom product from the second distillation zone contains from about 99.8 mol % to about 99.95 mol % ethyl acetate.

23 (amended). A process according to [any one of claims 20 to 22, in which] claim 20, wherein the second distillate comprises the overhead stream from the second distillation zone and is returned to the first distillation zone.

24 (amended). A process according to claim 23, [in which] wherein the overhead stream from the second distillation zone contains about 25 mol % ethyl acetate, about 68 mol % ethanol, about 6 mol % water, and about 1 mol % of other components.

25 (amended). A process according to claim 23 [or claim 24, in which] , wherein the overhead stream from the second distillation zone is returned to the first distillation zone at a point above the feed point of the liquefiable products of the selectively hydrogenated reaction product mixture.

26 (amended). A process according to [any one of claims 18 to 25, in which] claim 18, wherein in step (f) the ethanol rich stream recovered from the bottom of the first distillation zone is subjected to treatment for the removal of water therefrom thereby to produce a relatively dry ethanol stream suitable for recycle to step (a).

27 (amended). A process according to [any one of claims 1 to 26, in which] claim 1, wherein the relatively dry ethanol stream of step (f) is recycled to step (a).

28 (amended). A process according to [any one of claims 1 to 12, in which] claim 1, wherein step (e) comprises extractive distillation with an extractive agent comprising polyethylene glycol and dipropylene glycol, diethylene glycol, or triethylene glycol.

29 (amended). A process according to [any one of claims 1 to 12, in which] claim 1, wherein step (e) comprises extractive distillation in the presence of an extractive agent containing dimethyl sulphoxide.